

**Amendments to the Claims:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (Currently Amended) Method for treatment of spent liquor at a pulp mill, especially for treatment of black liquor, in order to recover its contents of chemicals and energy, wherein a spent liquor flow (10) arriving from the an evaporation plant is taken to a pyrolysis reactor (1), wherein it is pyrolysed at a temperature of 300-800°C in the absence of an external gas component in order to separate evaporable compounds (12) from the coke (11) remaining in a solid state, whereupon the evaporable compounds (12) are recovered and the coke (11) is taken to a gasification reactor (3) for gasification, which gasification is implemented under such conditions that the sulphur compounds contained in the coke (11) and deriving from the cooking chemicals are reduced to sodium sulphide.
2. (Previously Presented) Method according to claim 1, wherein only a part of the spent liquor flow (10) arriving from the evaporation plant is taken to the pyrolysis reactor (1), whereas a second part of the spent liquor flow (10) is taken to a soda recovery boiler (3) where it is burnt in order to recover its contents of chemicals and energy.
3. (Previously Presented) Method according to claim 1, wherein the evaporable compounds (12) separated from the spent liquor in the pyrolysis reactor (1) are used at the mill as fuel in part or entirely.
4. (Previously Presented) Method according to claim 1, wherein the evaporable compounds (12) separated from the spent liquor in the pyrolysis reactor (1) are processed further.
5. (Currently Amended) Method according to claim 1, wherein the product gases (14) resulting from the gasification are used at the mill as fuel in part or entirely.
6. (Cancelled)
7. (Previously Presented) Method according to claim 1, wherein the pyrolysis reactor (1) is for a batch process, whereby increasing of the temperature may begin from the temperature of

the spent liquor arriving in the reactor, while the final temperature is chosen according to the desired final products.

8. (Previously Presented) Method according to claim 1, wherein the pyrolysis reactor (1) is for a continuous process.
9. (Previously Presented) Method according to claim 1, wherein the pyrolysis is carried out in such process conditions (temperature, pressure, residence time, heating speed, etc.), wherein the evaporable compounds (12) mainly consist of non-condensing gases.
10. (Previously Presented) Method according to claim 1, wherein the pyrolysis is carried out in such process conditions (temperature, pressure, residence time, heating speed, etc.), wherein the evaporable compounds (12) mainly consist of pyrolysis oil.